

ESTROGENIC HORMONE REMOVAL FROM WASTEWATER USING NF/RO MEMBRANES

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ABSTRACT

This paper investigates the separation process of two estrogenic hormones, estrone and estradiol, using eight commercial NF and low pressure RO membranes. The results indicate that the separation mechanism of estrone and estradiol in membrane filtration processes is similar. While estrogenic hormone retention by porous membranes decreases with decreasing adsorption and the subsequent retention is relatively low, tight NF and RO membranes can retain estrogenic hormones effectively. It appears that the presence of organic matter in solution can enhance retention due to the interaction of such substances with estrogenic hormones. The results also suggest that physicochemical interactions within the membrane can play an important role. There is no cross flow effect on retention, whereas an increase in transmembrane pressure may lead to a decrease in steroid hormones retention for some membranes.

Keywords: *estrone, estradiol, endocrine disrupting chemicals (EDCs), nanofiltration, reverse osmosis, trace contaminants, membrane adsorption.*

1. INTRODUCTION

The public health and environmental implications of the so called "Endocrine disrupting chemicals" (EDCs) have been the subject of many scientific investigations, media interest and policy attention over the last few years. Hundreds of compounds, whose abundance in the aquatic environment have been identified, are known to be EDCs. There has been a mounting number of evidence of endocrine disrupting effects on laboratory animals and wildlife exposed to those chemicals such as fish [1-3], birds [4, 5], amphibians [6], and panthers [7]. Several researchers also suggest a link between environmental EDCs exposure and deteriorating trends in human health including decreases in male sperm count, increases in testicular, prostate, ovarian and breast cancer, reproductive malfunctions [8, 9], amongst more complex nervous, developmental and behavioural abnormalities [10]. Although, other researchers still caution about such a direct link and insist on more studies, it is now clear that fetus and new born babies are more vulnerable [10]. Public awareness and policy attention have recently spurred a number of studies investigating the fate and transport of EDCs in the environment, and particularly their removal in water and wastewater treatment processes.

Natural estrogenic hormones estradiol and estrone are by far the most endocrine disrupting chemicals. Their endocrine disrupting potency can be several thousands times higher than that of other synthetic chemicals such as nonyl phenol (see Table 1). Concentration as low as 1 ng/L of estradiol can result in a distinctive endocrine disrupting effect in male trout [1]. Estradiol controls the development of the female sex characteristics in humans and together with the gestagens, control the reproductive process [11]. In fact, 17 α -ethinylestradiol (a synthetic analogy of estradiol) is the main component of the contraceptive pill since it gives the same effect as this natural hormone. Under certain conditions, estradiol can be transformed into estrone.

Estrogenic hormones are continuously discharged by humans and animals into the environment either directly or after undergoing wastewater treatment processes, which are often not designed or capable of removing such contaminants. Removal efficiency of conventional wastewater treatment plants varies greatly [12]. Consequently, these hormones are ubiquitous in most fresh water bodies receiving effluent. They are frequently detected in North America, Europe, Japan, Brazil and China within the lower ng/L range [13-16]. A recent comprehensive study conducted by the US Geological Survey on fresh water resources across the US has revealed that the occurrence frequency of estradiol and estrone are about 10 and 7 % with maximum concentration up to 93 and 112 ng/L, respectively [15]. In particular, an estradiol concentration of 2.6 μ g/L in the South Nevada Water System, which provides drinking water to the city, has been reported [17]. Estradiol concentrations ranging from 6 to 66 ng/L have also been reported in groundwater (mantled karst aquifers in northwest Arkansas, USA) [18].

Although it is suggested that advanced technologies such as membrane filtration (reverse osmosis), advanced oxidation and activated carbon adsorption can effectively remove trace organic contaminants including estrogenic hormones [19], studies on the performance of such technologies with regards to hormone removal are still very limited. This can probably be attributed to the fact that until recently, there have been few analytical methods capable of quantifying these compounds at the required trace levels. Such methods are tedious, skill-demanding and still mostly limited to reconnaissance missions. Further, it will not be feasible in the near future to monitor such contaminants on a regular basis, especially in complex matrices such as wastewaters.

Applications of nanofiltration (NF) and reverse osmosis (RO) in the water industry are growing. NF and RO processes are particularly effective to remove trace contaminants

both inorganic (such as nitrate, arsenic and fluoride) [20, 21] and organic (such as pesticides and other synthetic organic chemicals) [22-24]. Removal of emerging wastewater pollutants namely pharmaceutical active compounds [25] and steroid hormones [26] has recently been studied at their environmental concentration (in the order of ng/L). However, such studies are still scarce and there is a need to further expand our understanding of the retention mechanisms of such low concentration contaminants in NF and RO membrane processes.

In previous works, we have studied the retention mechanisms of estrone by NF/RO membranes using bench scale equipment (stirred cells). The results indicate that estrone can adsorb onto the membranes to some extent, depending on membrane type and the solution chemistry [27]. Both sieving and adsorptive mechanisms are instrumental in maintaining high retention in nanofiltration membranes that otherwise exhibit relatively low ion retention [26].

In this study, using cross flow filtration equipment and eight different commercial NF/RO membranes, we reconfirm such findings and further elucidate other factors governing the retention of estrogenic hormones. Estrone and estradiol retentions were compared. The influence of other bulk organic matter in the solution on estrogenic hormone retention was examined. Finally, the study considers the effects of different operating variables namely cross flow velocity and transmembrane pressure on retention.

2. MATERIALS AND METHODS

2.1 Membranes

Eight commercial membranes were selected for this study, namely TFC-S, TFC-ULP, TFC-SR1, and TFC-SR2 supplied by Koch Membrane Systems (San Diego, USA) and X-20, ACM-4, TS-80, and XN-40 supplied by Trisep Corporation (Goleta, USA). It has been shown in our previous work that all membranes are negatively charged near pH neutral [26]. Hydrophobicity of the membranes is also described elsewhere [26].

2.2 Filtration System and Protocol

The cross flow filtration system includes a SEPA® cross-flow cell (Osmonics), a feed pump, a recirculation pump (Micropump), and a digital flowmeter. A picture of the system is shown in Fig. 1. The effective membrane surface area is 138.7 cm² (146 x 95 mm) and the channel height is 0.86 mm. Prior to the experiment with the cross flow system, the membranes were gently washed using DI water to remove the protective coating and a new membrane was used for each experiment. The membranes were compacted for at least 1 hour using DI water at 10 bar. Pure water flux was then determined at the end of the compaction process. The feed reservoir was then emptied and the system was drained out to avoid dilution. The feed reservoir was then refilled with the test solution. The applied pressure was 10 bar and both permeate and retentate were recycled to the feed reservoir, unless otherwise stated. Permeate and feed samples were collected for analysis at specified intervals.

Feed solution was prepared by spiking estrone or estradiol into a solution containing background electrolyte (20 mM of NaCl and 1 mM of NaHCO₃), synthetic surface water or secondary effluent solution to a concentration of 100 ng/L. This presents a typical concentration of natural hormones often encountered in domestic wastewaters while still ensuring analytical accuracy. A feed volume of 3.5 L was used for each experiment.

Retention is defined as: $R = 100 \times \left(1 - \frac{C_p}{C_f} \right)$, where C_p and C_f are permeate and feed concentrations (ng/L), respectively.

2.3 Solution Chemistry and Chemicals

All chemicals were of analytical grade. Radiolabelled estrone-2,4,6,7-³H(N) and estradiol-2,4-³H(N) (92 % purity) were purchased from Sigma Aldrich (Saint Louis, Missouri, USA). Secondary effluent was obtained from Brendale wastewater treatment plant in Queensland, Australia. Previous analysis showed that it contains about 10 mg/L total organic carbon (TOC), 50 mg/L of sodium and 10 mg/L of calcium [28]. Natural organic matter (NOM) was concentrated from Mooney-Mooney dam. Surface water using 10 mg/L of NOM in background electrolyte was used in this project. TOC was analysed by using a Shimadzu TOC-5000 instrument. The instrument was set on high sensitive catalyst and NPOC (non-purgeable organic carbon) analysis.

2.4 Natural Hormone Characteristics and Analysis

Estrone and estradiol have a very low solubility in water (see Table 2). Their K_{ow} values suggest their hydrophobic nature and moderate to high binding to colloids and macromolecules in water. Laboratory studies indicates that estrone and estradiol can adsorb moderately onto sediment [29]. The acid dissociation constant, pKa, of estrone is 10.4 [26]. Given the similarity in structure between the two compounds, it is expected that pKa of estradiol is also 10.4. Functional groups of estrone can facilitate the formation of hydrogen bonding between the molecule and the membrane surface. Theoretically, estrone can be either a proton-donor or a proton-acceptor species, while estradiol can only act as a proton-donor. Molecular structures of estrone and estradiol are shown in Fig. 2.

Estrone and estradiol were analysed using a Packard Instruments scintillation counter. This technique offered excellent accuracy with a detection limit of less than 0.1 ng/L.

3. RESULTS AND DISCUSSION

3.1 Retention of estrogenic hormone estrone

Retention of estrone by 8 different NF/RO membranes in the cross-flow system in a clean matrix solution (background electrolyte in DI water) is shown in Fig. 3. Although both sieving and adsorptive effects are instrumental in maintaining retention, for tight NF and RO membranes, size exclusion becomes the overriding mechanism and adsorption mostly occurs on the membrane surface [30]. In such circumstances, adsorption does not contribute to the overall retention of the membrane and this can be observed for the TFC-S, TFC-ULP, X-20, TS-80 and ACM-4 membranes.

Estrone retentions of the TFC-SR2, TFC-SR1, and XN-40 membranes decrease until equilibrium between estrone and the membrane has been established. Subsequent retention when stabilized is lower than the initial value. As reported previously, these membranes exhibit generally low ions retention. Sodium chloride retention of TFC-SR2, TFC-SR1, and XN-40 membranes are in the range between 2 to 17%, 24 to 32 % and 21 to 34 %, respectively [26]. The transport mechanism of estrone across these membranes can be characterized as convection dominated and both sieving and adsorptive mechanisms are effective in retaining estrone [27]. However, the membrane adsorptive capacity becomes exhausted over time as solution is filtered through the membrane, only sieving mechanism plays a role in long term retention.

This results in clear break-through curves similar to that which is in other adsorption processes such as activated carbon (see Fig. 4). For TFC-SR1 and XN-40 membranes, at the break-through point, the permeate concentration is far less than the initial feed concentration because of the sieving effect and depletion of estrone due to adsorption. Nishiyama et al., investigated the adsorptive interaction between estradiol and porous hollow fiber membranes (average pore size of 0.4 μm) and reported a similar break

through phenomenon [31]. However, at the point of break through, permeate concentration is equal to the feed concentration. This also shows that there is no sieving effect as the membrane pore size is much larger than the estradiol molecules.

3.2 Comparison of estrone and estradiol retention

Retention of estrone and estradiol in a clean matrix solution using TFC-S and TFC-SR2 membranes is shown in Figure 5. Although there are small differences between estrone and estradiol retentions, such differences are well within the experimental errors as reported (approximately 3%) in our earlier publication [26]. Estrone has a 17-keto group, whereas estradiol has a 17-hydroxyl group. Other than that, they have a similar molecular structure (see Fig. 2). The results indicate that the 3-oxygen atoms of the first ring of estrone and estradiol may predominantly participate in hydrogen bonding with the membrane polymer. This is consistent with the result reported by Le Questel *et al.*, [32] in their study of the hydrogen bonding formation between progesterone to its human receptor. Data reported in their study indicate that the 3-oxygen atom of progesterone is the predominant hydrogen bonding acceptor.

3.3 Effects of bulk organic matter

Organic compounds occur naturally and are ubiquitous in any aquatic environment where they often determine the surface properties of any solids in contact with water. Organic matter found in water spans a wide spectrum, their molecular weight ranging from several hundred thousands to less than a hundred Daltons (grams per mol). While natural water contains compounds mostly on the lower end of this spectrum, secondary effluent contains even lower molecular weight organics as they have been broken down during biological treatment processes. Although bulk organics are not considered harmful to human health, they are relevant the precursor for the formation of carcinogenic trihalomethanes (THMs) and other disinfection by-products after disinfection. Further, as contaminants like estrone can bind to organic matter, their presence can enhance retention and generally determine the fate of compounds. Finally, some fraction of organic matter may compete with estrone for adsorptive sites. Consequently, this competition can also affect retention where adsorption is a dominating factor.

To study the effects of organic matter on estrone retention, experiments were conducted in three different matrix solutions: pure background electrolyte matrix, secondary effluent, and synthetic surface water (natural organic matter concentrated from Mooney Mooney Dam in background electrolyte). Ionic strengths of the clean matrix and the synthetic surface water were prepared to be approximately that of secondary effluent. Likewise, the organic content of synthetic surface water was selected to be identical to that of secondary effluent (TOC = 10 mg/L).

Estrone retentions in the different matrix solutions by X-20, TFC-S and TFC-SR2 membranes are shown in Fig. 6A, B, and C, respectively, whereas TOC retention in secondary effluent is shown in Fig. 7. It appears that estrone retention is enhanced by the presence of organic matter. Furthermore, this enhancement seems to be stronger for natural water than in secondary effluent (containing organic matter of smaller molecular weights). Large molecules can be retained more effectively, hence, exert a stronger influence on estrone retention. However, this phenomenon is not observed for TFC-SR2 membranes, possibly due to its larger pore size. Reported results are consistent with an earlier study by Agbekodo *et al.*, [33] who investigated the influence of natural organic matter concentration on atrazine and simazine retention by the NF-70 membrane. An increase in atrazine and simazine retention as a function of organic matter concentration in the feed solution was reported.

3.4 Comparison of cross-flow and dead-end filtration

Although the application of dead end filtration configuration using NF or RO membranes is not common as it is prone to fouling, the simplicity of dead end filtration equipment such as stirred cells makes them a preferable testing tool for many membrane researchers. In contrast to cross-flow filtration, recovery in dead-end mode can be very high, which results in a significant concentration factor and can represent the recovery effect on concentration inside real life modules very well. Fig. 8 shows the comparison between cross flow and dead end filtration. Experiments using a stirred cell were conducted in an earlier study [30], where a series of fresh estrone solutions (100 ng/L) were consecutively filtered through a single TFC-S membrane sample to examine if membrane saturation could be achieved.

While retentions are in agreement for a permeate volume of up to 200 mL, as the permeate volume increases retention obtained from the stirred cell starts deviating from that of the cross flow cell. In dead end filtration, a volume of permeate is drawn from the feed solution without any replenishment, which results in a continuous increase in feed concentration in the cell. As fresh estrone solutions are repeatedly introduced to the stirred cell, estrone retention increases in each dead end filtration cycle due to the difference in concentration at the end and the beginning of the next one. At the end of each filtration cycle estrone is accumulated on the membrane surface, which results in a greater chemical gradient for the transport of estrone across the membrane. It has been proved that diffusion rate of aromatic compounds such as bisphenol A and 2-chlorophenol in dense membrane can be relatively fast if the compounds are readily to partition into the membrane polymer [34]. The results indicate that dead end filtration test may underestimate the long term retention of the membrane. The effect of operating variables such as cross flow velocity and transmembrane pressure are consequently investigated in the following sections.

3.5 Effects of operating variables

Understanding the impact of operating variables on retention of trace contaminants is of paramount importance from design as well as operational points of view. The influence of cross-flow velocity and operating pressure on estrone retention was examined in this study. The XN-40 membrane was selected as it exhibits medium range estrone retention. To eliminate the influence of adsorption, the membrane was equilibrated with estrone solution in background electrolyte matrix for 5 hours at 10 bar. Cross-flow velocity was then varied from 0.073 m/s to 0.24 m/s. A fresh solution was used to examine the operating pressure effects on retention. After equilibrating the membrane with the same procedure, the pressure was varied from 10 to 25 bar. Three samples at each cross-flow velocity or operating pressure were taken for analysis at an interval of 15 minutes.

Estrone retention as a function of cross-flow velocity is shown in Fig. 9. An increase in cross-flow velocity can reduce the polarization concentration at the membrane-bulk solution interface. The effect could lead to an increase in retention. However, no cross-flow velocity effects on estrone retention can be observed in this study. As estrone adsorbs onto the membrane surface, the estrone concentration within the membrane can be higher than that of the polarization layer. Therefore, the polarization concentration effect appears in this case negligible.

The results are different for a variation in operating pressure. Fig. 10 shows that estrone retention decreases by 15% as the pressure increases from 10 to 25 bar. In general, solute retention increases with pressure up to an asymptotic value. However, for organic solutes that have strong interaction with membrane polymers, retention may decrease with pressure [35]. It has been reported that retentions of chlorophenol [36], chloroform [37], and nonyl phenol [38] decrease as pressure increases. Interestingly, these contaminants were similarly reported to be able to adsorb to the membrane. While the results are

consistent, a plausible explanation is to date not available and our hypothesis is that pressure influences the membrane-solute interactions.

Solute membrane interactions can be friction (governed by hydrodynamic conditions) and diffusion (governed by chemical concentration gradient). The average pore diameter of the XN-40 membrane was determined to be 0.7 nm followed a method described elsewhere [39], which is in the same order of magnitude as the molecular size of estrone, such interactions can be critical. An increase in pressure results in an increase in permeate flux; and hence the drag force within the membrane pores also increases. Consequently, desorption of estrone can be enhanced or time for adsorption reduced due to the lowers residence time in the membrane which may contribute to the drop in retention. In addition, an increase in pressure will also lead to an increase in permeate recovery, which further reduces the retention.

4. CONCLUSIONS

The separation process of two estrogenic hormones estrone and estradiol was investigated using eight commercially available NF and low pressure RO membranes. Results reported here indicate the similarity between estrone and estradiol with regards to separation in membrane filtration. Depending on the pore size, adsorption can affect the transport of estrogenic hormones across membranes. While tight NF and RO membranes can effectively retain estrogenic hormones, retention of porous membranes (TFC-SR2, TFC-SR1 and XN-40) decreases as adsorption decreases illustrating a breakthrough curve, and the subsequent long-term retention of these three membranes is relatively low. The presence of organic matter appears to enhance hormone retention. This enhancement is apparently stronger in natural water, in which organic matter generally has larger molecular weight, than that in secondary effluent. Cross flow is more effective than the dead end configuration, probably due to lower adsorption. There is no cross flow effect on retention, whereas an increase in operation pressure results in a decrease in hormone retention. Both of these are most likely linked to the membrane – solute interactions observed.

5. ACKNOWLEDGEMENT

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Figure 1: Cross flow filtration equipment.

Figure 2: Molecular structure of estradiol (left) and estrone (right).

Figure 3: Retention of estrone by 8 NF/RO membranes (10 bar, 1 mM NaHCO₃, 20 mM NaCl, cross flow velocity of 0.073 m/s, pH ~ 8).

Figure 4: Estrone concentration in permeate by TFC-SR1, TFC-SR2, and XN-40 membranes as a function of time (10 bar, 1 mM NaHCO₃, 20 mM NaCl, cross flow velocity of 0.073 m/s, pH ~ 8).

Figure 5: Estrone versus estradiol retention (10 bar, 1 mM NaHCO₃, 20 mM NaCl, cross flow velocity 0.073 m/s, pH ~ 8).

Figure 6: Estrone retention in different matrix solution by X-20 (A), TFC-S (B) and TFC-SR2 (C) (10 bar, cross flow velocity of 0.073 m/s, pH ~ 8, surface water and secondary effluent solutions contain 10 mg/L organic matters).

Figure 7: TOC retention in secondary effluent (10 bar, cross flow velocity of 0.073 m/s, pH ~ 8).

Figure 8: Estrone retention by TFC-S membrane during dead end and cross flow filtration (10 bar, 1 mM NaHCO₃, 20 mM NaCl, cross flow velocity of 0.073 m/s, pH ~ 8).

Figure 9: Estrone retention as a function of cross flow velocity (XN-40 membrane, 1 mM NaHCO₃, 20 mM NaCl, pH ~ 8).

Figure 10: Estrone retention as a function of operating pressure (XN-40 membrane, 1 mM NaHCO₃, 20 mM NaCl, cross flow velocity of 0.073 m/s, pH ~ 8).

Figure 1



Figure 2

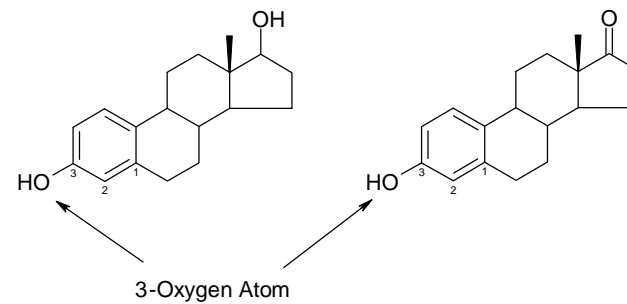


Figure 3

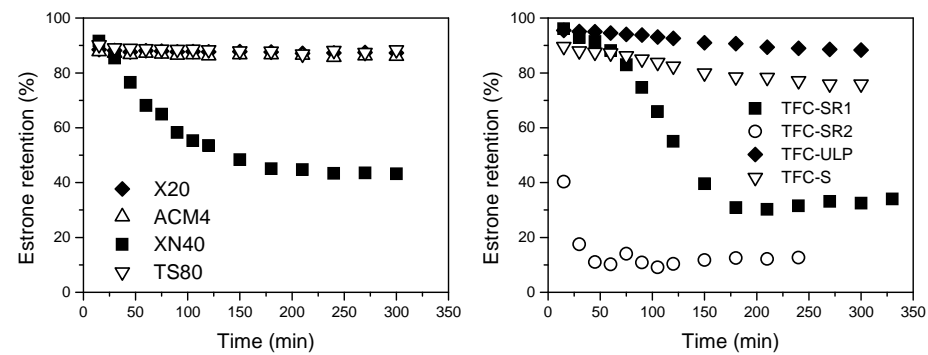


Figure 4

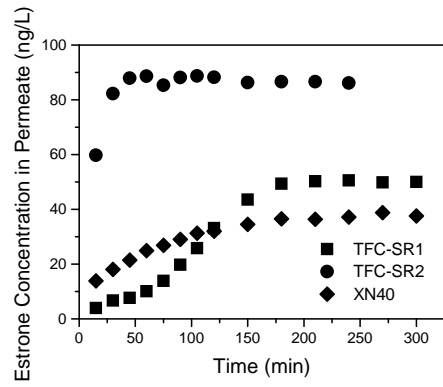


Figure 5

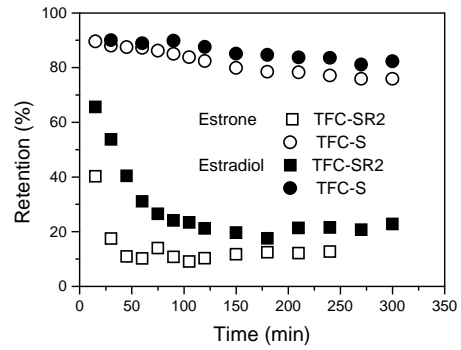


Figure 6

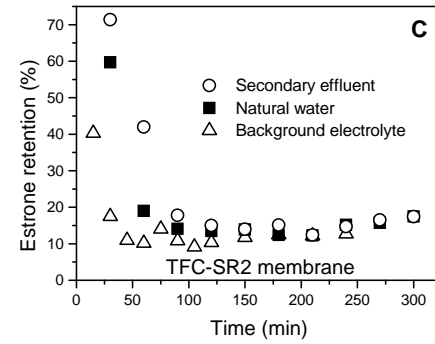
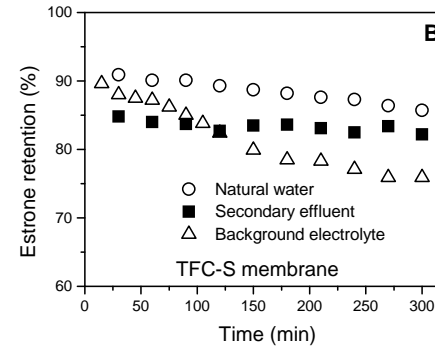
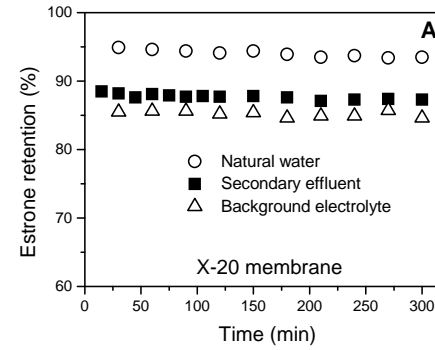


Figure 7

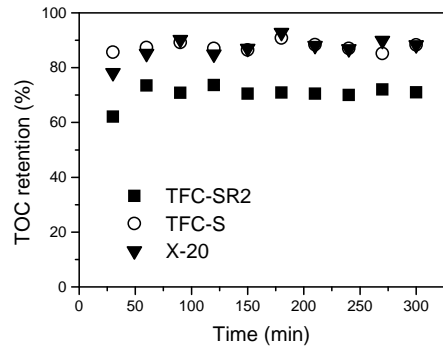


Figure 8

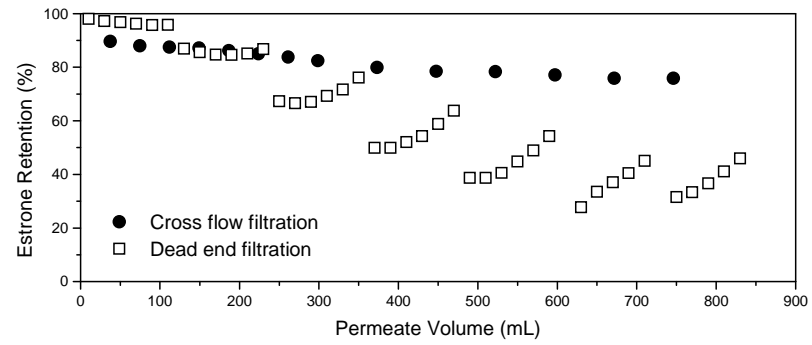


Figure 9

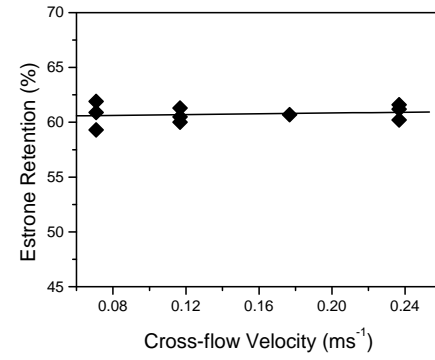


Figure 10

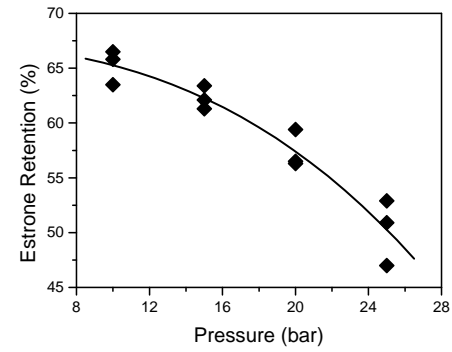


Table 1: Examples of endocrine disrupting potency in relation to estrone and estradiol.

Substance	Relative potency	Reference
Estradiol	1	[40]
Estrone	1	
Progesterone	2×10^{-2}	
Testosterone	1×10^{-2}	
Phytoestrogens	$< 1 \times 10^{-3}$	[41]
4-Nonyl-phenol	9×10^{-6}	

Table 2: Physicochemical properties of estrogenic hormones

Hormones	Molecular weight	Water solubility at 20 °C ^a	pKa ^b	log K _{ow} ^a
Estradiol	272.4 g/mol	13 mg/L	10.4	3.94
Estrone	270.4 g/mol	13 mg/L	10.4	3.43

^a [29]

^b [26]